#### The Design of a Family of Process Compressor Stages

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## Outline

- Objectives
- Master and Derived Stages
- 1D Design Guidelines
- Detailed design
- Manufacture and Testing
- Summary





# Multistage inline compressors

- Used in a wide range of volume flows, pressure ratios and gas properties for different applications
- Use families of pre-engineered stages to meet individual customer's requirements by changing
  - Impeller diameter
  - Number of stages
  - Stage types
  - Speed
  - Cooling arrangement
- Overall performance is calculated by stage-stacking of the individual stage characteristics
- Penalties for 'failure' quite high







# **Objectives**

- Upgrade the performance of the existing compressor family at Howden ČKD Compressors
- Choice of master stages and a series of derived stages to adapt these to the exact flow conditions required
- Cover a range of flow coefficient ( $\phi = \frac{4V_0}{\pi U_2 D_2^2}$ ) between 0.0075 and 0.15
- Preliminary and detailed design of the stages
- Performance testing of selected stages





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• For a fixed first stage, the flow coefficient of the downstream stages varies depending on the machine tip speed Mach number  $(M_{u_2} = \frac{U_2}{\sigma_{u_2}})$ 

$$\phi_{n+1} = 4\dot{m} / (\rho_{t2}\pi D_2^2 u_2) = (\rho_{t1} / \rho_{t2})\phi_n = \frac{\phi_n}{\left(1 + (\gamma - 1)\lambda M_{u2}^2\right)^{1/(n-1)}}$$



- Col Charles Renard was a designer of airships for the French Army in the 1880's
- He proposed the system of 'preferred' numbers that became ISO 3
- Used it to reduced the number of different balloon ropes kept on inventory from 425 to 17
- It divides a decade into 5, 10, 20 or 40 steps



Col. Charles Renard (1847-1905)

- Step change in flow coefficient was determined by the Renard R40 series
  - 6% ( $\sqrt[40]{10}$ ) change in flow coefficient between successive stages
  - 60 stages to cover the entire range from 0.0075 to 0.15
- Derived stages are trimmed from master stages to achieve intermediate stages



- Designing new stages for each application is not practicable
- Seven master stages were used to cover the required flow range
- The step size can be smaller at high flow coefficients stages and larger at low flow coefficients
  - Rotordynamic advantage in switching earlier to shorter low flow coefficient stages
  - Efficiency drop at high flow coefficients (or more sensitive to trimming)





- Trim profiles were determined from the calculated streamlines in the 2D throughflow calculation of the original master stage to achieve similar
  - Aerodynamic loading
  - Inlet and outlet flow angles
  - Incidence





3D st	ages:	142000.0051 22 App 20111 Stopp new optimum with pits (m = 0.09	
	Master	Derived	0.4 0.35
A3	$\phi_{M} = 0.1500$	0.1400, 0.1320, 0.1250	0.3
<i>B</i> 3	$\phi_M = 0.1180$	0.1120, 0.1060, 0.1000, 0.0950	
<i>C</i> 3	$\phi_{M} = 0.0900$	0.0850, 0.8000, 0.0750, 0.0710, 0.0670	
<i>D</i> 3	$\phi_{M} = 0.0630$	0.0600, 0.0560, 0.0530, 0.0500, 0.0475, 0.0450	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
<i>E</i> 3	$\phi_M = 0.0425$	0.0400, 0.0375, 0.0355, 0.0335, 0.0315, 0.0300, 0	).0280

#### 

How

#### 2D stages:

	Master	Derived	
- <u>A2</u> -	$\phi_{M} = 0.0630$	<del>0.0600, 0.0560, 0.0530, 0.0500, 0.0475, 0.0450</del>	0 0.05 0.1 0
<i>B</i> 2	$\phi_{\!M}=0.0425$	0.0400, 0.0375, 0.0355, 0.0335, 0.0315, 0.0300, 0.0280	
<i>C</i> 2	$\phi_{\!M}=0.0265$	0.0250, 0.0236, 0.0224, 0.2120, 0.0200, 0.0190, 0.0180	
<i>D</i> 2	$\phi_{\!M}=0.0170$	0.0160, 0.1500, 0.0140, 0.132, 0.0125, 0.0118, 0.0112	
		0.0106, 0.0100, 0.0095, 0.0085, 0.008, 0.0075	



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# Impeller

- Impeller **axial length** increases in high flow coefficient stages
- Previous guideline by Aungier

 $\frac{L_{imp}}{r_2} = 0.08 + 3.16\phi$ 

 Current guideline results in shorter high flow coefficient stages

$$\frac{L_{imp}}{r_2} = 0.1 + 2\phi$$

• Typically 0.6-0.7 for turbocharger and gas turbine impellers (cf 0.4 from the above equation)





# Impeller

• Impeller eye radius ratio

$$\frac{r_{ic}}{r_2} = 0.5 + 1.5\phi$$

Impeller hub radius ratio

$$\frac{r_{ih}}{r_2} = 0.35$$

Impeller outlet width ratio

$$\frac{b_2}{r_2} = 0.05 + 0.8\phi$$

• 10-20% pinch in the diffuser, determined in the detailed design





#### Diffuser

- Diffuser radius ratio of 1.6 to reduce the kinetic energy at inlet to the crossover bend
- Vaneless diffusers at high and medium flow coefficients
  - Wider operating range

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#### Diffuser

• Vaned diffuser at low flow coefficient stages:

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- High loss generation in excessively narrow diffuser passages
- larger impeller tip widths have been used to widen the passage
- Vaned diffusers have been used to avoid possible flow instabilities and high losses associated with high flow angles in vaneless diffusers





## **Return Channel**

- Accelerating flow from deswirl outlet to the inlet of the downstream impeller to avoid possible flow separations
- $b_{rc_out}$  depends on the flow coefficient of the downstream impeller ( $\phi_{n+1}$ )
- $\phi_{n+1}$  depends on the density ratio and hence on the tip speed Mach number ( $M_{u2}$ ) of the upstream stage

$$\phi_{n+1} = 4\dot{m} / (\rho_{t2}\pi D_2^2 u_2) = (\rho_{t1} / \rho_{t2})\phi_n = \frac{\phi_n}{\left(1 + (\gamma - 1)\lambda M_{u2}^2\right)^{1/(n-1)}}$$

- A return channel designed for high  $M_{u2}$  results in excessive deceleration at low speed
- Return channel width is typically larger than the diffuser width







## **Return Channel**

• From the guidelines presented before it can be shown:

$$b_{rc_out} / r_2 = \left(\frac{A_o}{A_i}\right) \left(\frac{r_2}{Rr_{ic}}\right) \left(\frac{\left[(r_{ic} / r_2)^2 - (r_{ih} / r_2)^2\right]}{2}\right)$$

• 
$$R = \frac{r_{rc\_out}}{r_{ic}} = 1.25 - 1.35$$

- Smooth bend at the inlet
- $A_0/A_i$  =1.25 to 1.35
  - 25% to 35% acceleration upstream of the impeller







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# Design process



#### Parameterised geometry generation of flow channel

3D stages at high φ







#### 2D stages at lower φ



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#### Parameterised geometry generation of flow channel

• Flow channel of full stage modelled with Bezier curves set up as patches

$$\vec{R} = (1-u)^3 \vec{P}_0 + 3u(1-u)^2 \vec{P}_1 + 3u^2(1-u)\vec{P}_2 + u^3 \vec{P}_3$$



- Vista GEO
  - Based on method of Casey (1983)
  - Similar system system as used in ANSYS Bladegen
  - Links to throughflow, mechanical analysis and to ANSYS bladegen



# Geometry generation of blades



# Throughflow calculations (Vista TF)

- Streamline curvature solution on a mean S2 surface
- Stanitz and Prian (1952) approximation for the blade to blade variation:

$$\frac{W_s - W_p}{r\Delta \vartheta} = 2\Omega \frac{\partial r}{\partial m} \cos \beta + W \cos^2 \beta \frac{\partial \beta}{\partial m} + \frac{\sin^2 \beta \cos \beta}{r} \frac{\partial}{\partial m} (rW)$$



• Experience-calibrated loading parameters:



• 9-stage, real gas calculation (extent of our experience)







- Detailed optimisation is based on 3D CFD calculations:
  - Single passage steady state calculations
  - Structured grid in bladed passages using ANSYS Turbogrid (ATM)
  - Effect of fillets and leakages can be ignored in the initial design loop
  - Unstructured mesh for complex parts (larger mesh size)



- Calculations using CFX 17.1 with SST turbulence model
- Mesh size typically 4m nodes (3.5m in impeller, diffuser and leakage paths)
- Compared to typically 250k nodes for a 'design' iteration (using k- $\epsilon$ )





Commercial-in-Confidence

How

#### Efficiency as a function of flow coefft.



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#### **Impeller** Vanes

- All shrouded impellers
- 2D vanes for the lower flow range ( $\phi \leq 0.046$ )
  - Brazed impellers
  - Brazing plane decided based on stress analysis
- 3D vanes for the high and medium flow range
  - Single-piece milled impellers
- operating tip-speeds up to 380 m/s (X5CrNi) were tested
- 500 m/s is possible with the use of titanium alloys









# **Performance Testing**

- Newly built, dedicated test facility at Howden ČKD Compressors (DARINA)
- The master stages were tested along with their smallest trim or derived stages at a range of tip speed Mach number from 0.3 to 1.1
- Detailed flow measurements were taken at five planes at impeller inlet, impeller outlet, diffuser outlet, return-channel inlet and return-channel outlet
- More than 120 pressure and 50 temperature probes were used
- Kiel probes, 3-hole probes and high frequency pressure transducers







- Fillets and leakages need to be included for accurate prediction of performance
- Large effects of the leakage flow on efficiency at low flow coefficients





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# Summary

- The design of a new family of process compressor stages using modern design methods has been described.
- The guidelines for preliminary design of the stages has been presented and aspects of the detailed design discussed.
- The test results show that the performance objectives have been achieved and the design tools have been effective
- Comparison of the CFD and test results confirm that the inclusion of real geometry features is necessary to obtain good agreement with the measured performance



